

Interreg

North Sea Region

NuReDrain

European Regional Development Fund



EUROPEAN UNION

NuReDrain Webinar II:

P recovery and P removal modelling

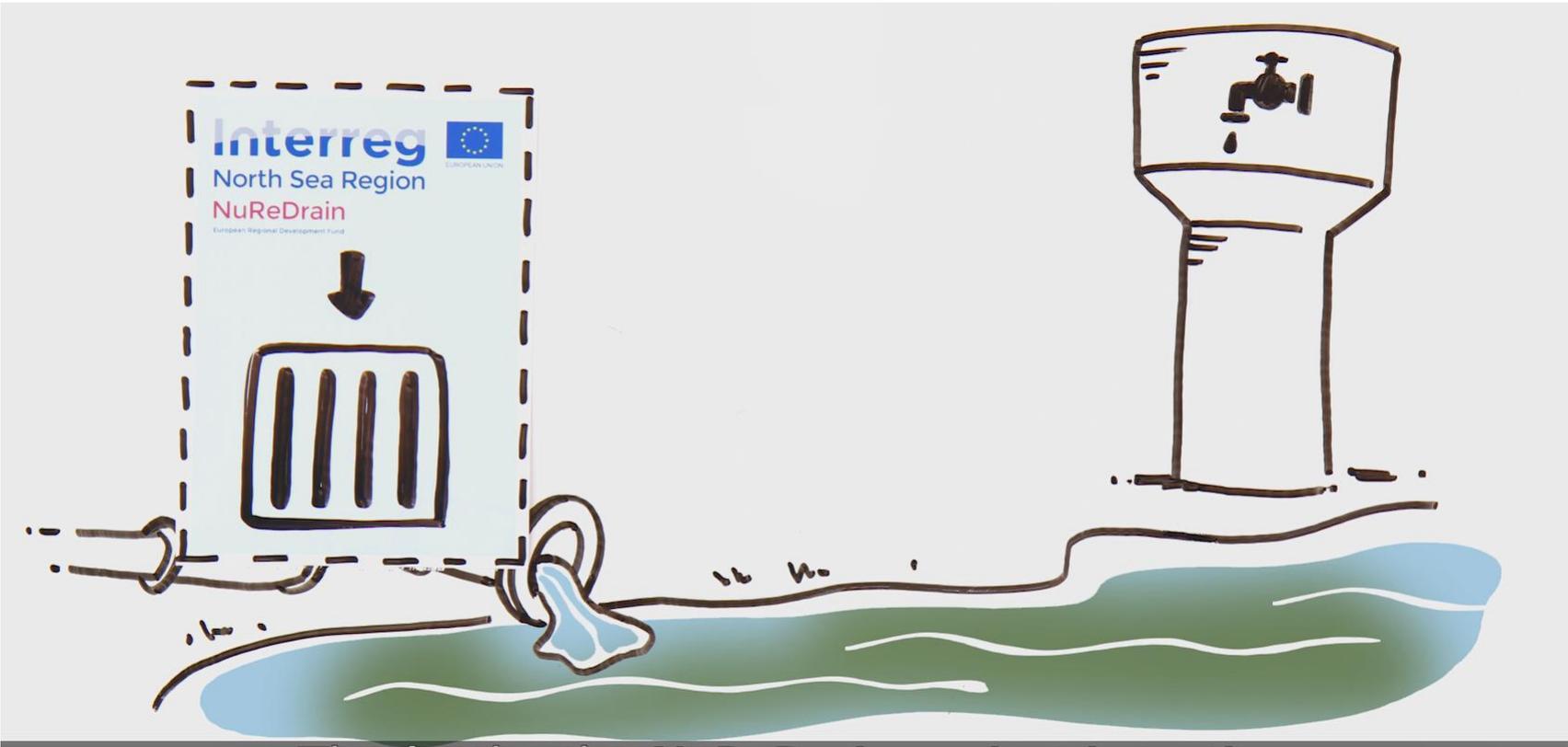
Practical issues

- Please mute yourself.
- Feel free to ask questions in the chat.
- The webinar will be recorded.
- Handouts will be put available afterwards.

- Nutrient Removal and Recovery from Drainage water
- 1/3/2017 – 30/9/2021
- Interreg North Sea Region
- Project cost: € 2 674 405 - Fund: € 1 337 203
- 11 partners in 3 countries



Project goal



Project goals

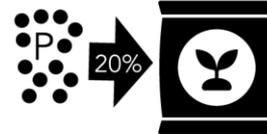
PROJECT GOALS



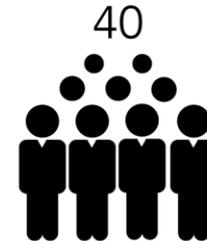
FILTER SYSTEMS ABLE
TO REMOVE 50% OF
N (= NITROGEN)



FILTER SYSTEMS ABLE
TO REMOVE 70% OF
P (= PHOSPHORUS)



20% MATERIAL
REUSE AS P-FERTILIZER



40 ORGANIZATIONS
ADOPTING FILTER
SYSTEMS

Agricultural waters

drainage water



greenhouse effluent



surface water

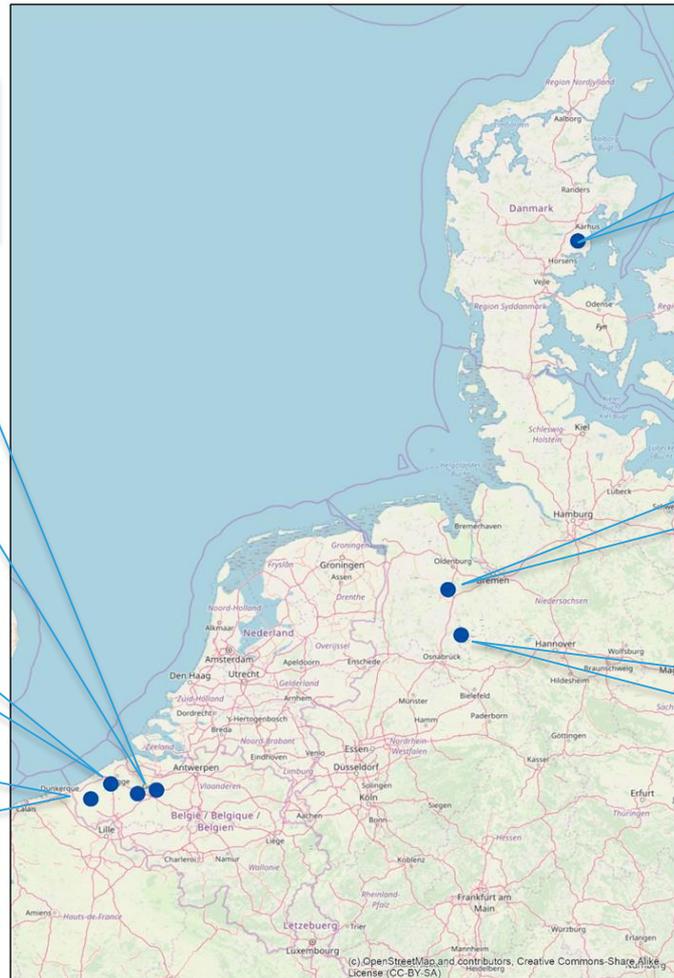


NuReDrain

water reservoir for drinking
water production



6 field cases



Greenhouse effluent
N + P removal

Drainage water
P removal

Water reservoir
P removal

Drainage water
N + P removal

Surface water
N removal

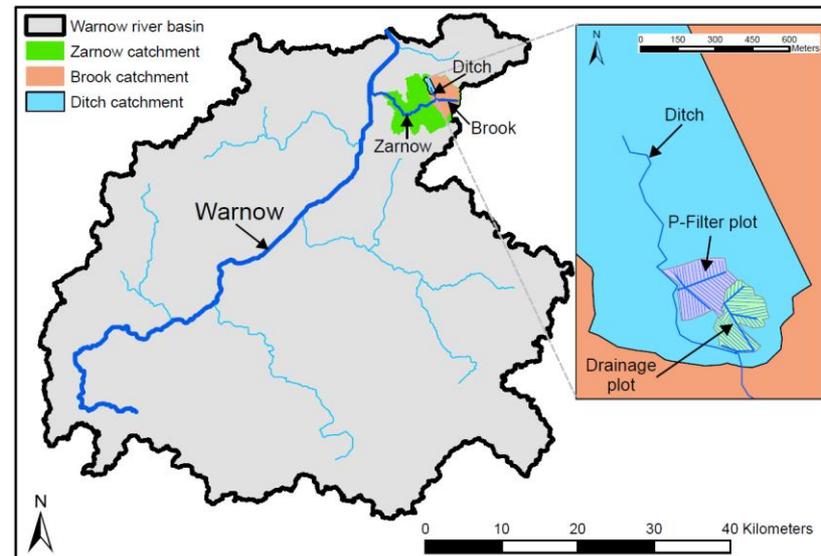
Drainage water
P removal

P recovery



Integration of P-adsorbing material in a circular process

Modelling





Reuse of saturated filter materials as fertilizer for ornamentals and vegetables

Els Pauwels

Ornamental Plant Research (PCS), Belgium

Problem statement

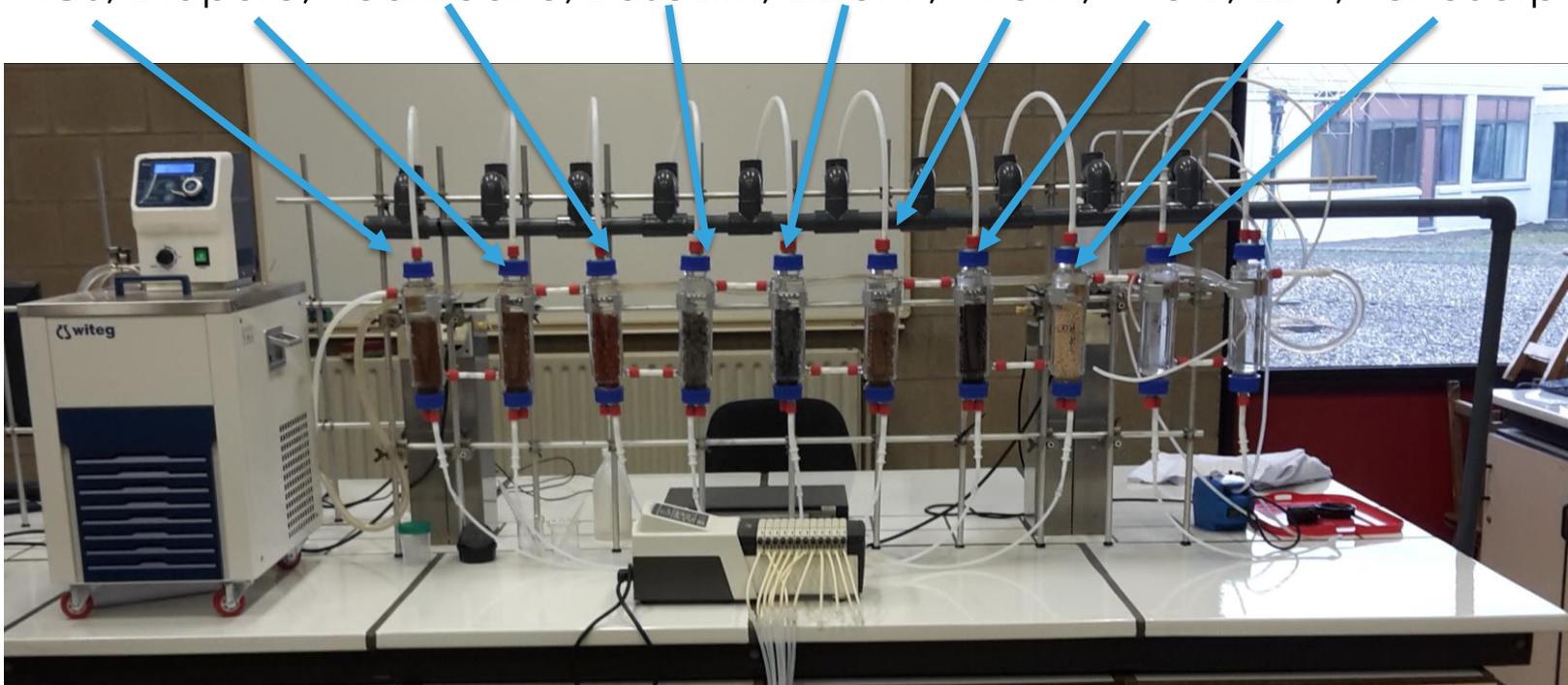
- Phosphorus recovery potential



P-removal – Column tests

- $\text{PO}_4\text{-P}$ solution: 0.5 ppm P
- Bed height: 14 cm \Rightarrow corresponds with a bed volume of 150 mL
- Temperature: 20 °C
- Flow rate: 0.66 L/24 h

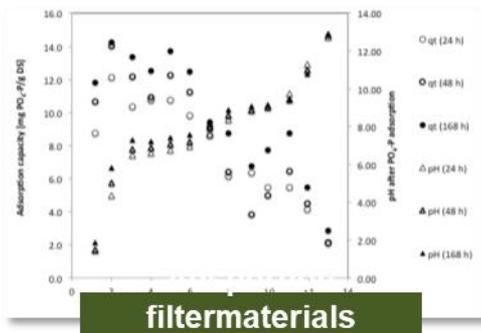
ICS, Diapure, Redmedite, BaseLith, LiDonit, Vito A, Vito B, LDH, FerroSorp



Problem statement

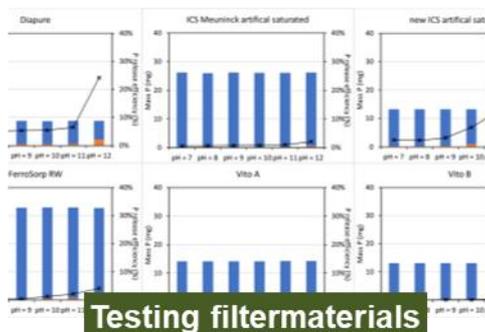
Available: ICS (Iron coated sand) :

- Waste product from drinking water production
 - Good removal of P - rich drainage waters
 - High conductivity of filters (depending on size of particles)
 - (Sufficiently) available and (relatively) cheap
-
- Reuse as a fertilizer without treatment?



Pot trial 2017:

- On azalea
- Low pH
- From ICS, there was almost no natural desorption of P, a little desorption of N
- Plants with ICS were of a lower quality compared with the control due to a P shortage



Trial PCS 2018: Buxus, Lavendula and Hedera

Table: Overview N and P dose for each tested species

	Treatment 1			Treatment 2			Treatments 3		
	Standard N and Standard P			Standard N without P			Standard N without P but with 30% ICS granules		
	N (g/l)	P ₂ O ₅ (g/l)	K (g/l)	N (g/l)	P ₂ O ₅ (g/l)	K (g/l)	N (g/l)	P ₂ O ₅ (g/l)	K (g/l)
Lavendula	420	245	665	420	0	663	420	0	663
Buxus	625	315	420	623	0	414	623	0	414
Hedera	525	315	420	537	0	414	537	0	414

Growth with standard N and standard P best

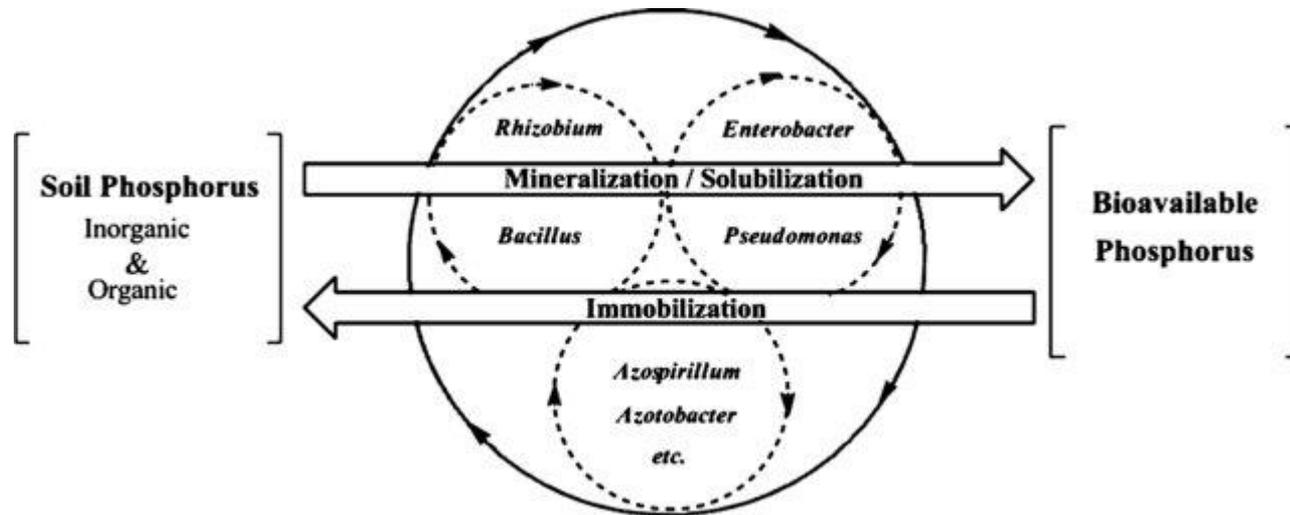
No phytotoxicity effects

Difficult to remove ICS grains for analysis

Trial PCS 2018: Buxus, Lavendula and Hedera



Schematic diagram of soil phosphorus mineralization, solubilization and immobilization by rhizobacteria



- Predominant bacterial PSB's (sharma et al, 2013):
 - Pseudomonas spp.
 - Bacillus spp.
- P – SOLUBILIZING POTENTIAL depends on :(Sharma et al, 2013)
 - Iron concentration in the soil
 - Soil temperature
 - C and N sources available

Trial PCS 2019: Hedera



Trial PCS 2019: Hedera



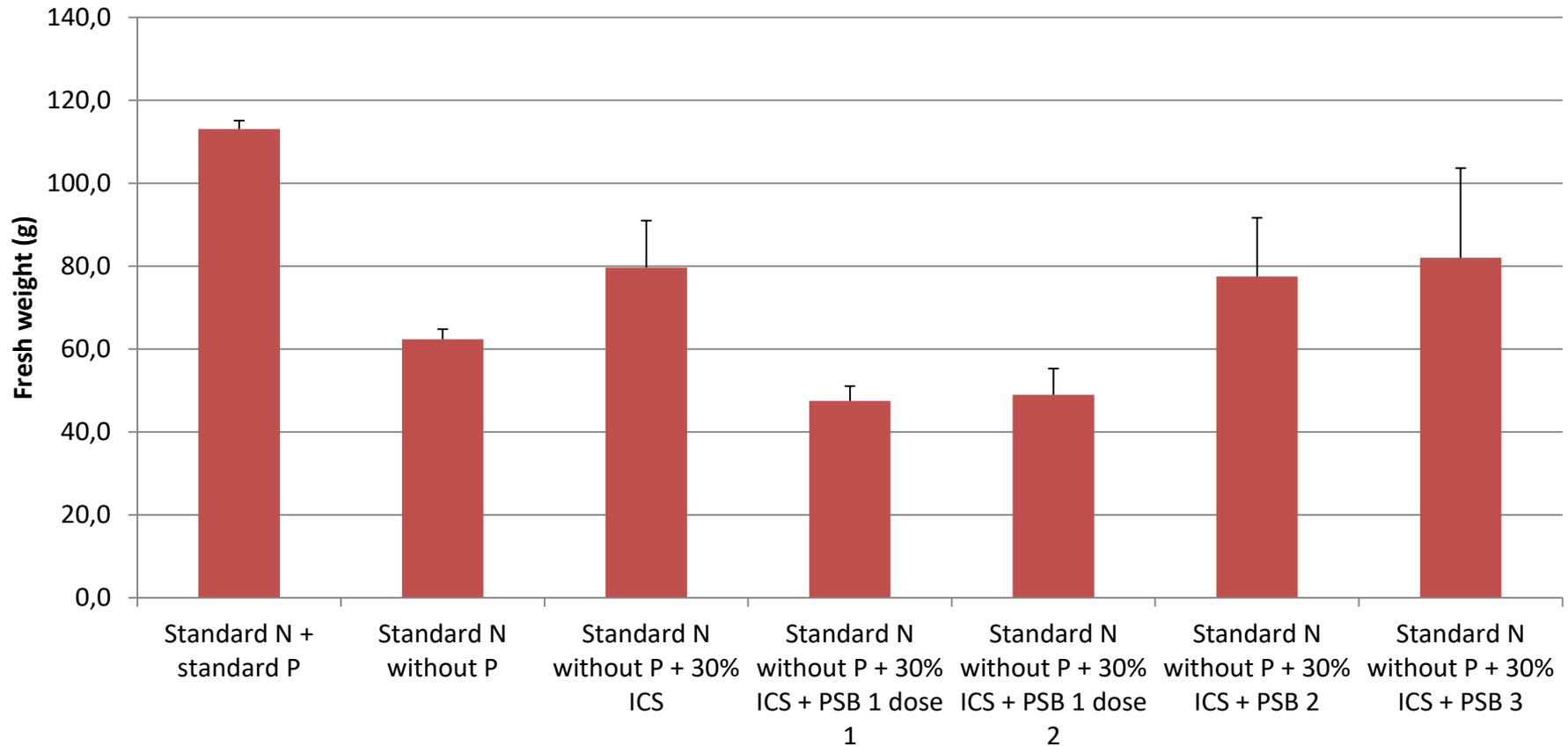
Treatment	
1	Standard N and Standard P
2	Standard N without P
3	Standard N without P but with 30% ICS granules
4	Standard N without P but with 30% ICS granules + dose 1 of PSM1
5	Standard N without P but with 30% ICS granules + dose 2 of PSM1
6	Standard N without P but with 30% ICS granules + dose 1 of PSM2
7	Standard N without P but with 30% ICS granules + dose 1 of PSM3

Potting: End of May
1,5 L pot
Open air

Trial PCS 2019: Hedera



Trial PCS 2019: Hedera



Endive:

growth chamber experiment + pot experiment

Use of ICS as a P – fertilizer

Use of PSB's

Evaluation of commercial products

Maize:

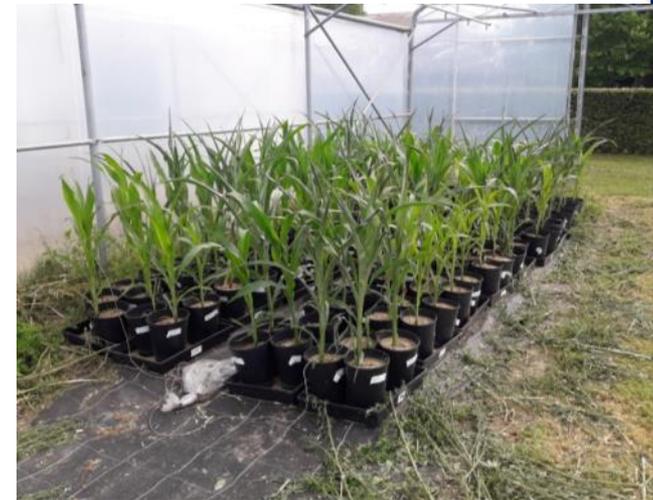
Pot experiment

Evaluation of commercial products

Pot trial maize P-fertilisation with ICS

Phosphorous fertilization value of P-saturated ICS in combination with PSB (P-solubilizing bacteria) in maize

1. Control (untreated)
2. APP (ammonium polyphosphate) = reference
3. TSP (triple superphosphate)
4. PT mix + ICS
5. PT mix
6. PT mix + TSP
7. Pseudomonas putida + ICS
8. Pseudomonas putida
9. Pseudomonas putida + TSP



Overall conclusion pot trials endive and maize

- -> fertilisation treatments with TSP or APP have significant the highest relative yield
- -> no positive effects of the use of PSB's in combination with ICS
- No indication that phosphorus rich material (ICS) has a potential as P-fertilizer
- No added value of PSB's in combination with ICS



Other possibilities to use ICS?

- Against slugs?



- Ironmax Pro (2,4% iron phosphate) (10721P/B),
- SluXX (3% iron phosphate) (9722P/B),
- Derrex (3% iron phosphate) (9904P/B)

Trial PCS: 14 different plant species

Azalea indica 'Fluostern'

Calluna vulgaris 'Siska'

Camelia

Chamaecyparis lawsoniana Elwoodii

Chrysanthemum 'Salomon Surfer mauve and *Chrysanthemum*

Sevilla orange bicolor "Josevor"

Erica x darleyensis 'kramer's rood'

Euonymus fortunei 'Emerald Gaiety'

Hydrangea paniculata 'Phantom'

Lavendula angustifolia 'Munstead'

Pelargonium zonale Dark 'Clara White'

Petunia surfinia var. Purple

Rhododendron ponticum 'Graziella'

Thuja occidentalis 'Brabant'

Waldsteinia ternata

Trial PCS: 14 different plant species



Trial PCS: As addition to the substrate? Chlorophytum

- Evaluation at end of trial (16/07/2018)



rooting 5 (left) – rooting 7 (right)

	# rootings trough pot	rootscore 1-7	Fresh weight (13 plants)	Visual plant quality
With ICS	8,3	6,2	333,13	9
Without ICS	8,5	6,2	310,37	9

Trial PCS: As addition to the substrate?

- Evaluation at end of trial

Chlorophytum



left without ICS – right with ICS

- **Chlorophytum**



left without ICS – right with ICS

- **Chrysanthemum**



- **Petunia**



Trial PCS 2020: ongoing

20 plants/treatment

- 1. Control
- 2. 30% ICS grains
- 3. 30% pellets



Trial 2020





Other possibilities to use ICS?



Standard·N·+·standard·P



Standard·N·without·P



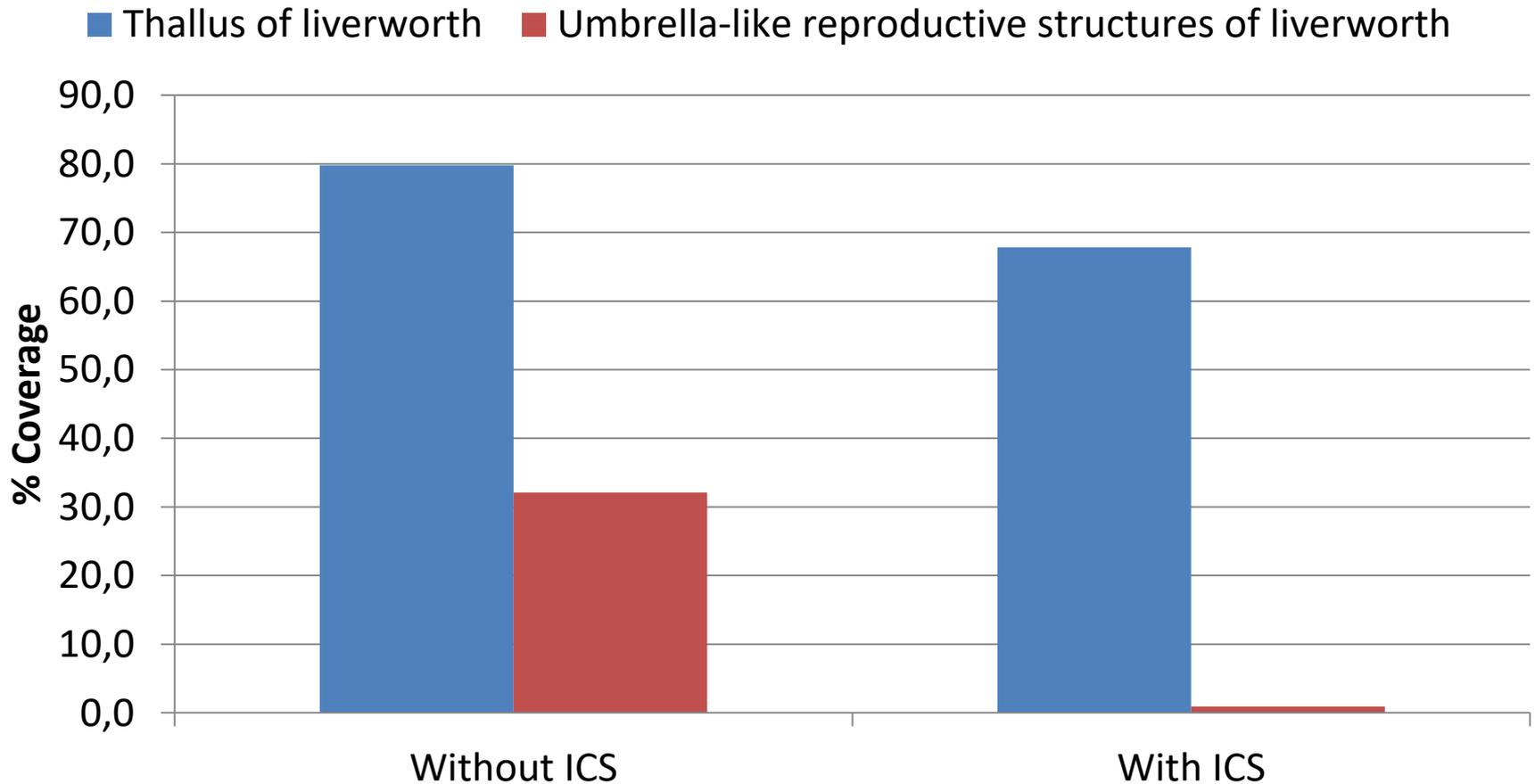
Standard·N·without·P·+·30%·ICS

Other possibilities to use ICS?



Other possibilities to use ICS?

Camellia



Other possibilities to use ICS?

- As a cover material?



Other possibilities to use ICS?



Other possibilities to use ICS?





- <http://northsearegion.eu/nuredrain/>
- Subscribe to our newsletter: <https://northsearegion.eu/nuredrain/news/>
- Els Pauwels- els.pauwels@pcsierteelt.be -+32 9 353 94 88

Interreg

North Sea Region

NuReDrain

European Regional Development Fund



EUROPEAN UNION

Webinar II: Recovery of phosphorus by chemical treatment

Nico Lambert – KU Leuven
Process & Environmental Technology Lab
KU Leuven

KU LEUVEN

Introduction

- Water flows from agriculture, e.g.,
 - Drainage water originating from tile drained agricultural fields
 - Greenhouse effluent
- contain phosphate amounts of unused fertilizers
- above the standard limits for surface water

Proposed solution:

Adsorption technology using Al and Fe based P-adsorbing materials: Iron Coated Sand (ICS), Vito A and B, DiaPure.

Relevant research question:

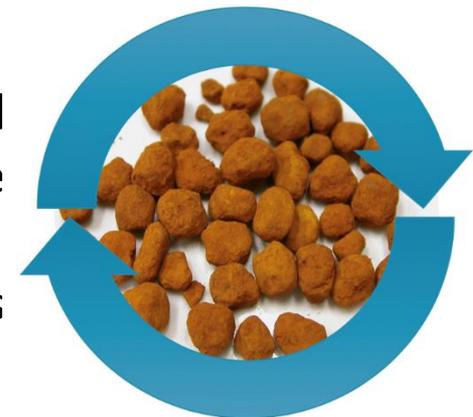
What about the saturated adsorption material: should it simply be disposed of as solid waste? When is recovery/regeneration recommended?



Integration of P-adsorbing material in a circular process

Prospects for P-recovery:

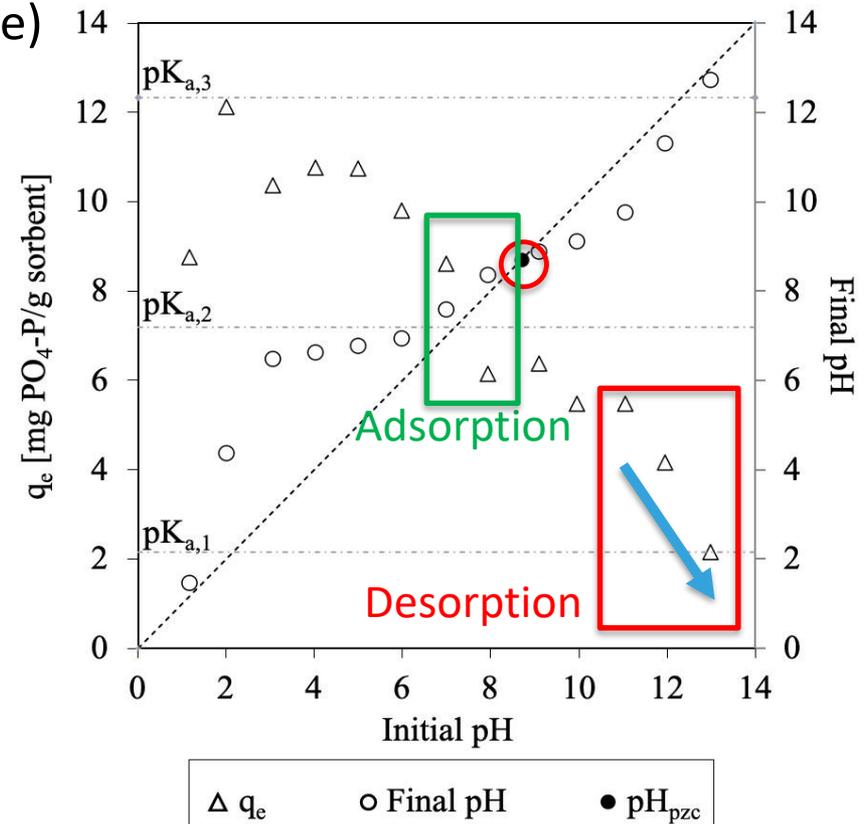
- The main objectives:
 - **Regeneration of the saturated sorbents** making it reusable in several adsorption/desorption cycles and
 - **Recovery of phosphorus** by precipitation or used directly with irrigation water as fertilizer .
- The reusability of the granules is as important (or even more) than recovering phosphate
- Different desorption reagents: inorganic and organic acids, chelating agents and alkaline solutions, are already proposed in the literature
- A desorption process using an **alkaline** solution is proposed without harming the adsorbing material.



Integration of P-adsorbing material in a circular process

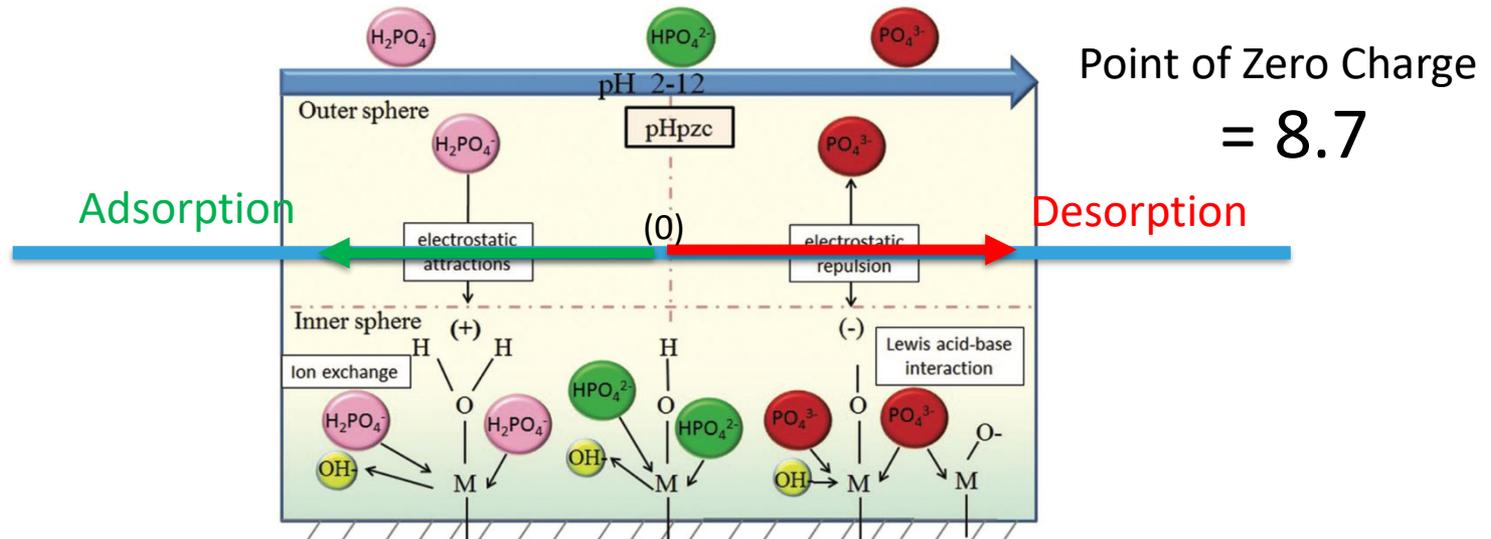
Theoretical basis:

- The influence of initial pH on the adsorption capacity q_e for ICS
- Adsorption/desorption are **balancing processes** until an equilibrium is reached!
- $\text{pH } 8.7 = \text{pH}_{\text{PZC}}$ (Point of Zero Charge)
= final pH is equal to the initial pH
- pH range 1 - 8.7: high q_e
- pH range 8.7 – 13: low q_e
- $\text{pH} > 11$ the q_e drops considerably



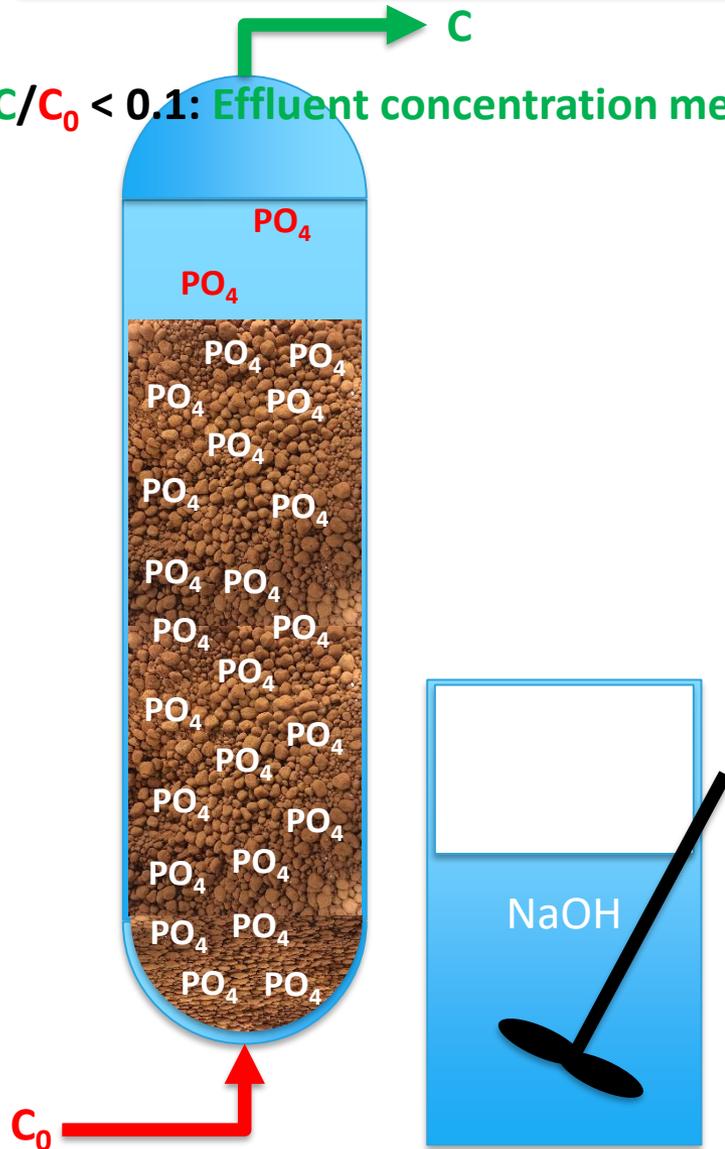
Theoretical basis:

- Li et al. (2016): higher pH = the phosphate adsorption is affected by
 - the electrostatic repulsion (surface is negatively charged) and
 - increasing competitive effect of OH⁻ ions for the active sites on the sorbent
 - =decreased adsorption capacity.

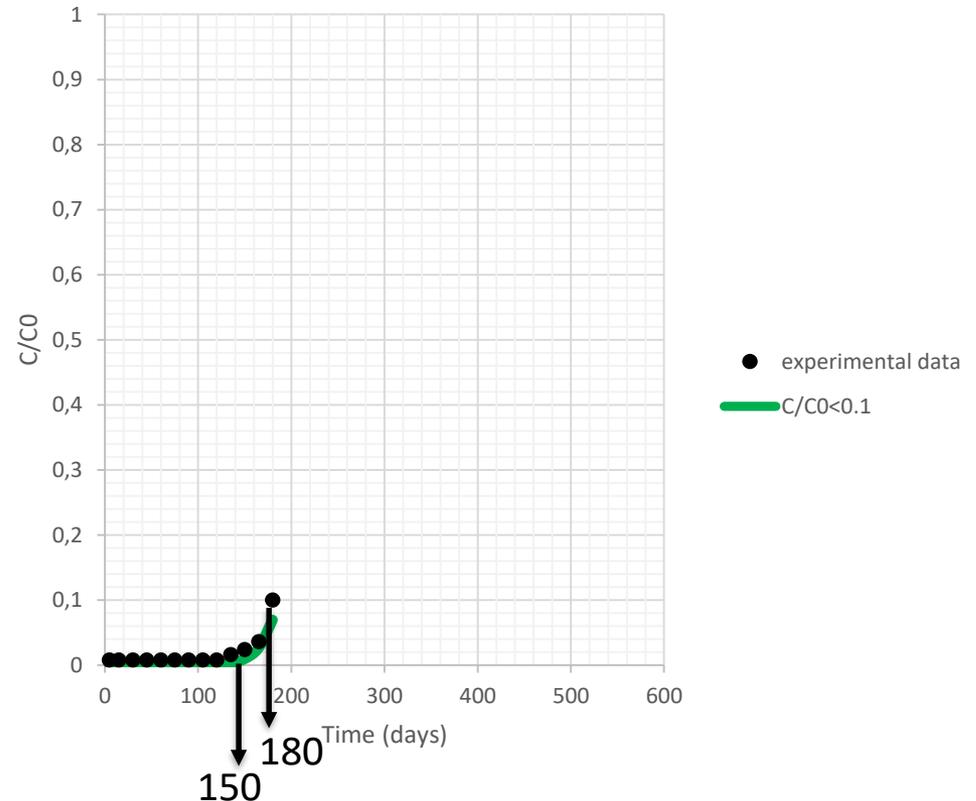


Concept of ad/desorption

$C/C_0 < 0.1$: Effluent concentration meets the discharge limit



Adsorption Phase: Day 0-180

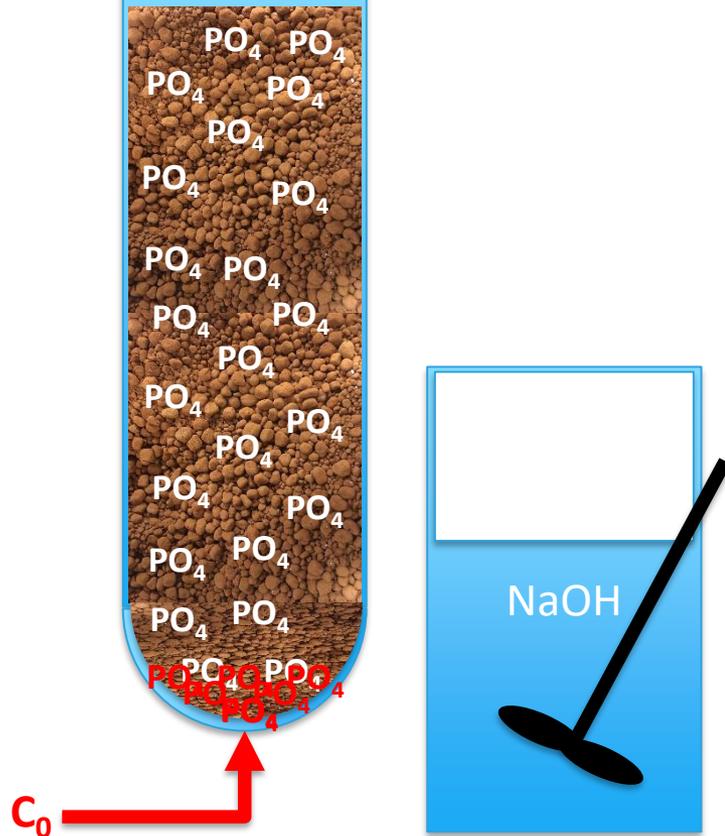


Concept of ad/desorption

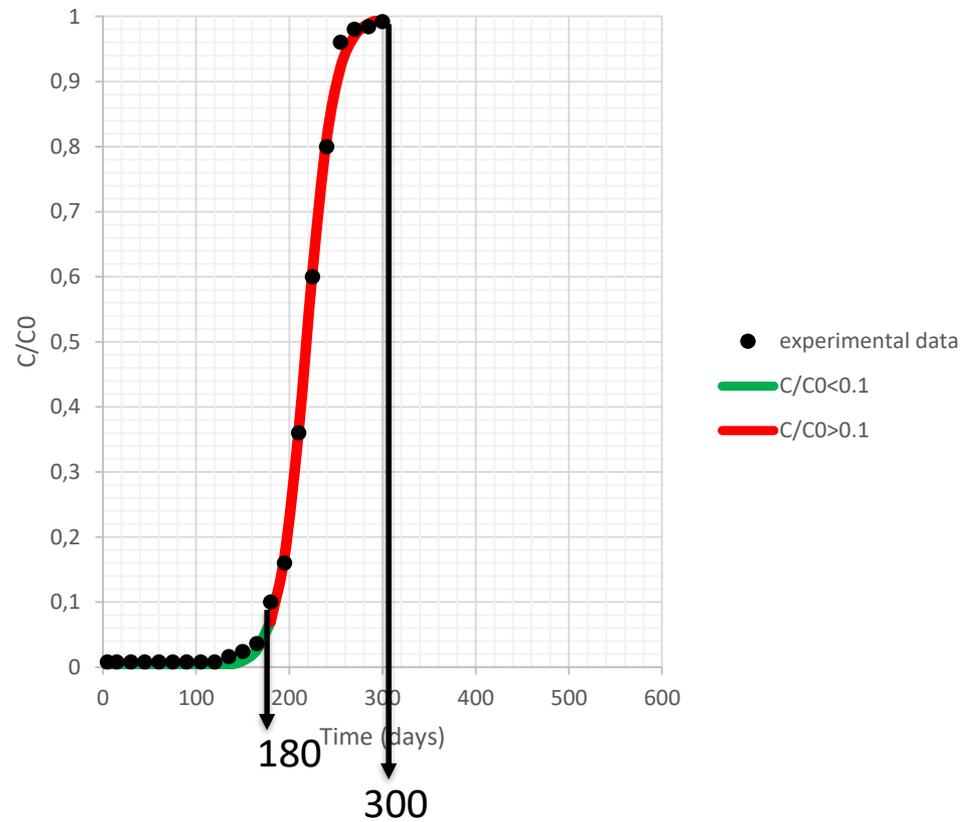


$C/C_0 = 1$ @ day 300: Adsorption material (ICS) is completely saturated

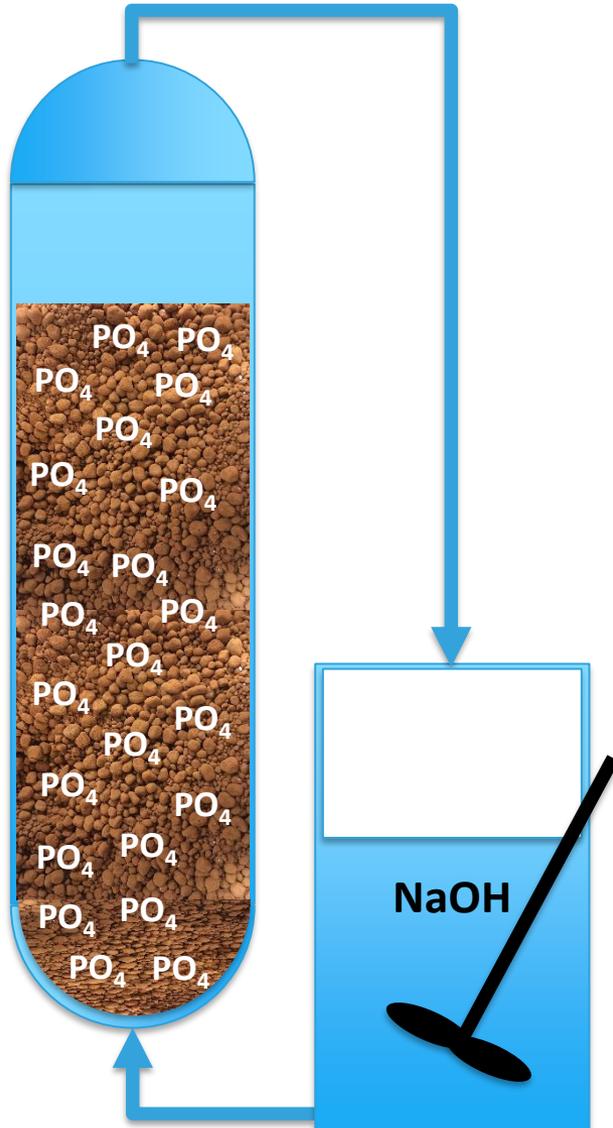
$C/C_0 > 0.1$ @ day 180: Regeneration of ICS is needed



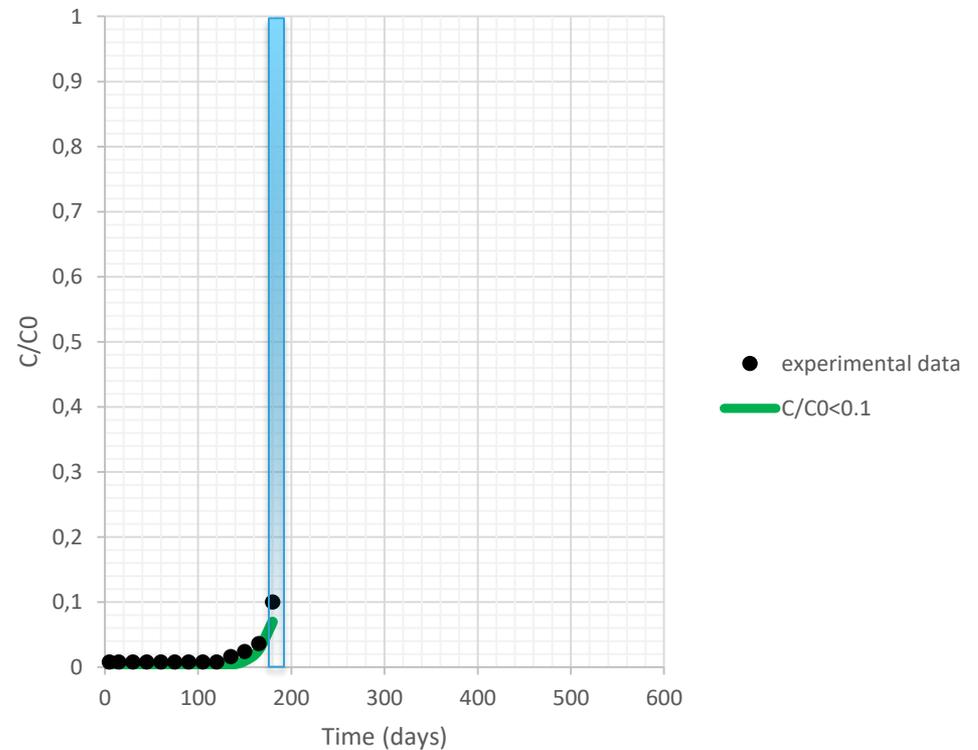
Adsorption Phase: Day 180-300



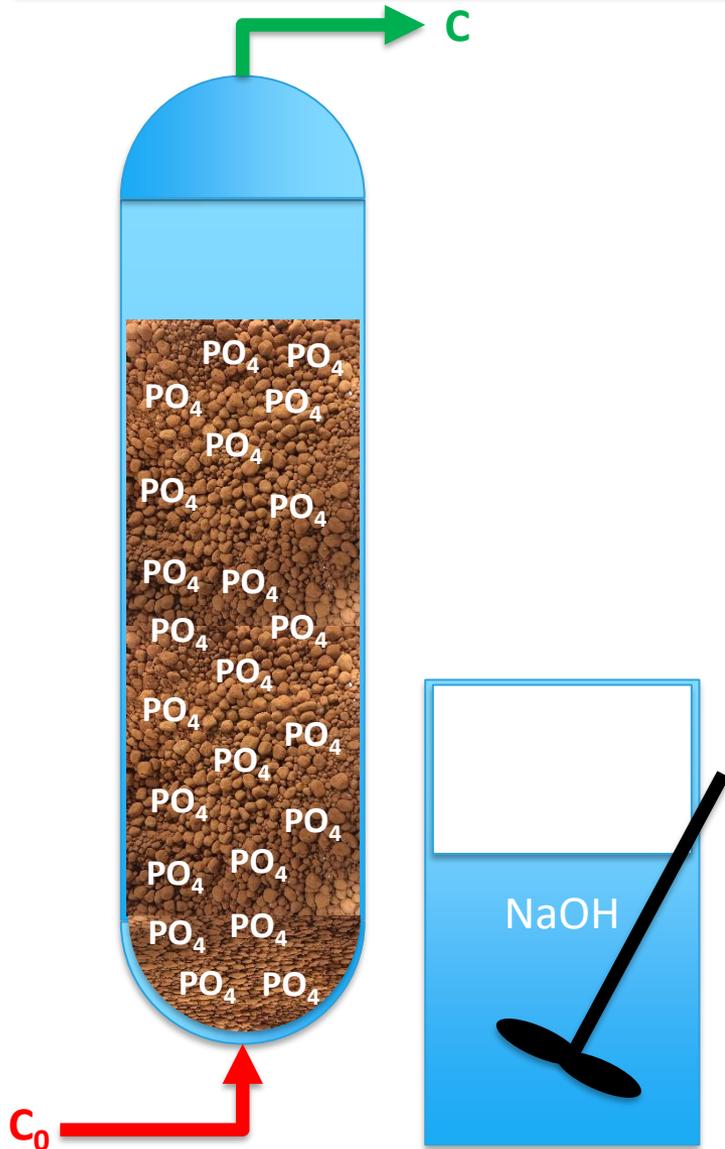
Concept of ad/desorption



Desorption Phase: Day 180

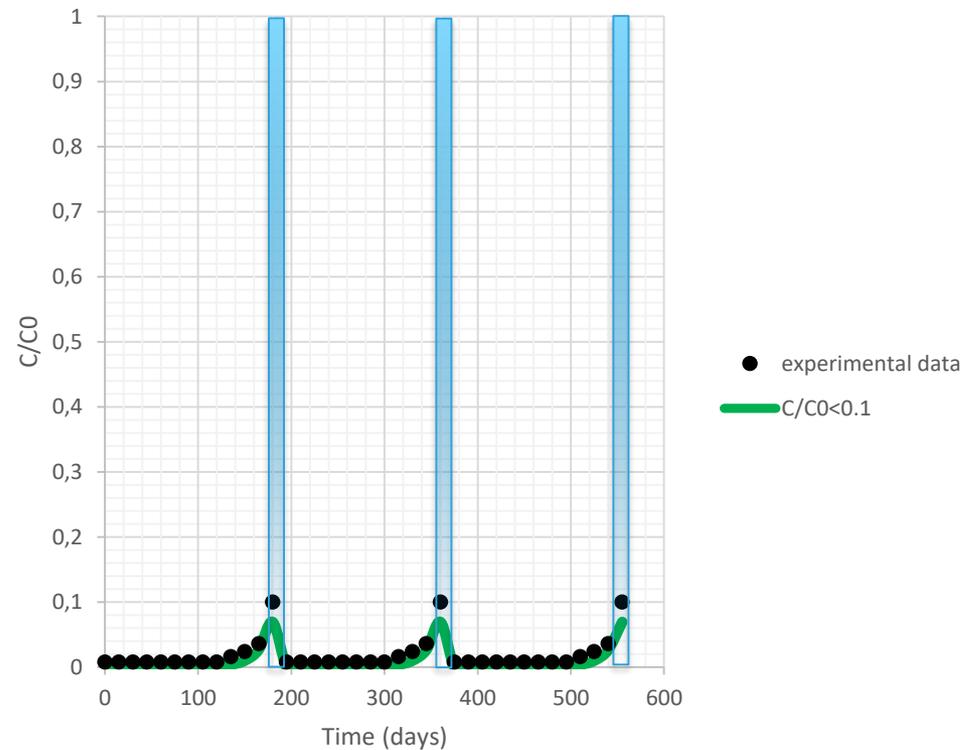


Concept of ad/desorption



Regeneration of the saturated sorbent and recovery of phosphorus

Intermittent regeneration of ICS



Materials & Methods

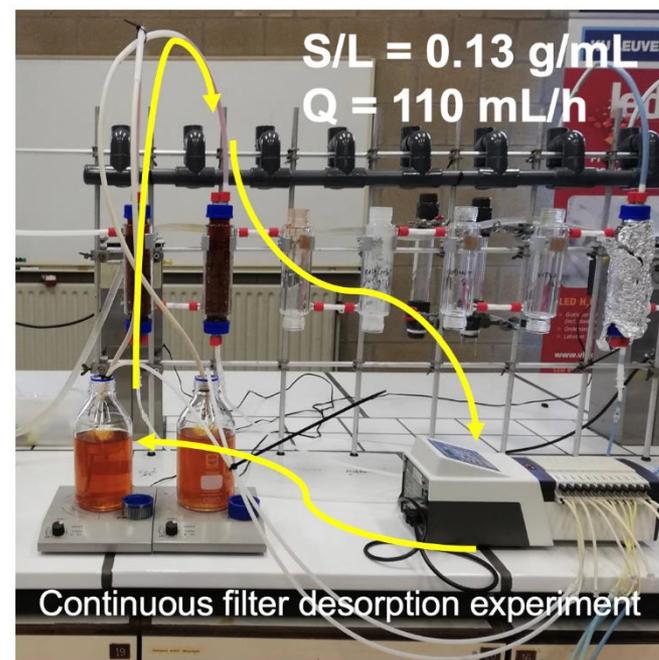
1. **Batch desorption experiments:** 5g of pre-dried saturated ICS was brought into contact with NaOH solution.

Variable parameters:

- NaOH concentration (1-0.5-0.1- 0.01- 0.001M),
- Desorption time (5min-48h)
- Solid/liquid ratio (S/L= 0.03-1 g/mL)

2. **Continuous filter desorption experiment:** 1 liter of NaOH solution was recirculated over an adsorption column filled with 128 g of saturated ICS granules.

3. **Analysis of the samples:** **Liquids:** $\text{PO}_4\text{-P}$ determination by ion chromatography after .45 μm filtration. **Solid grains:** SEM-EDX



Results & Discussion

Batch experiments

- The composition of 1 g of saturated ICS granules was determined by a complete destruction of the granules by Aqua Regia and ICP analysis:
 - Phosphorus: 15.30 +/-1.25 mg P/g DS =**1.5%P**
 - Iron: 590.7 +/-8.7 mg Fe/g DS =**59%Fe**

- Figure 1:** A minimum desorption time of 24 hours and a NaOH concentration of 0.1 - 1M is necessary to ensure a sufficiently high desorption efficiency.

- Figure 2:** The solid over liquid ratio (S/L expressed in g/mL) has a pronounced effect on desorption efficiency. An S/L lower than 0.10 g/mL is recommended.

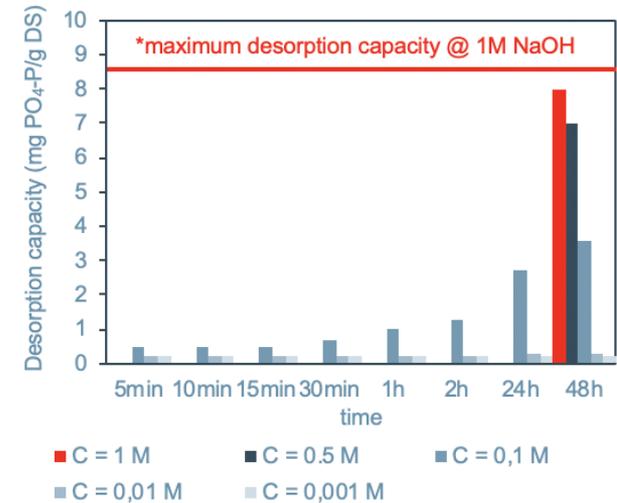


Figure 1: Influence of NaOH concentration and desorption time.

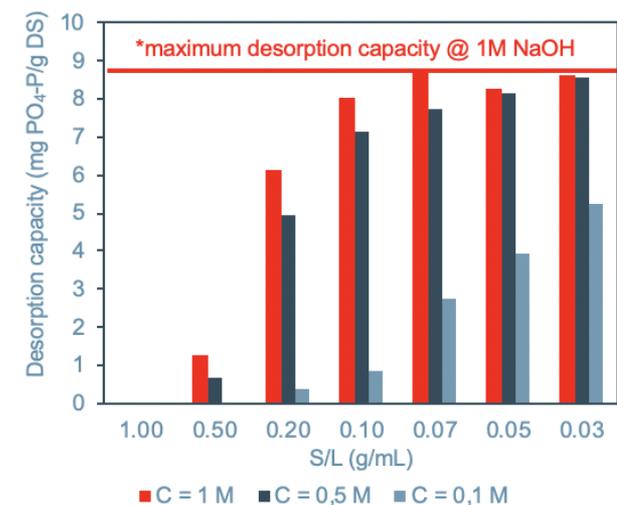


Figure 2: Influence of solid/liquid ratio.

Results & Discussion

Continuous filter experiments

- **Figure 3:** Continuous desorption filter experiments show that only a concentration of 0.5 and 1M NaOH lead to a desired desorption of phosphorus from the ICS granule. At least 24 hours desorption time must be provided.
- **Figure 4:** During the first hour of the continuous desorption experiment only 0.4 mg P/g DS and 0.9 mg P/g DS can be leached for a NaOH concentration of 0.5 and 1M respectively. A concentration of 0.1M NaOH desorbed almost no phosphorus.

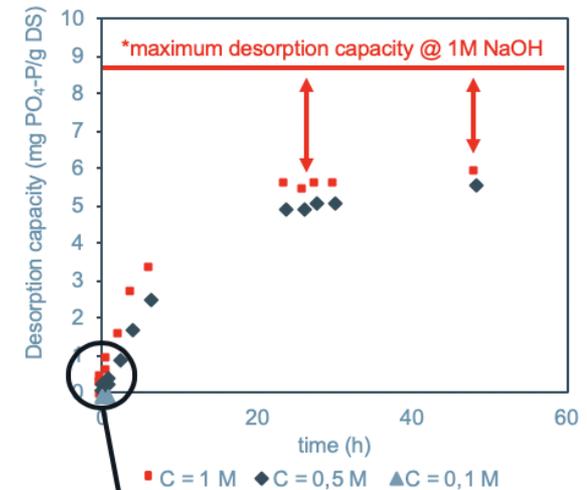


Figure 3: Continuous filter desorption experiment and the effect of the NaOH concentration on desorption capacity

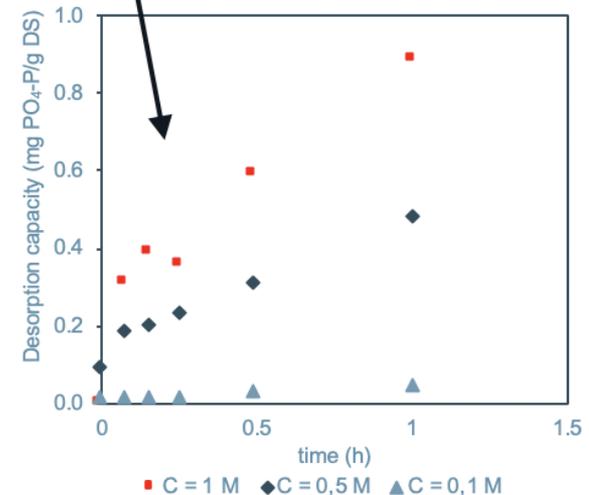


Figure 4: The progress of the desorption during the first hour of the continuous filter desorption experiment

Results & Discussion

SEM-EDX analysis

- Energy-dispersive X-ray (EDX) Analysis with a Scanning Electron Microscope (SEM) of saturated ICS from two column experiments.

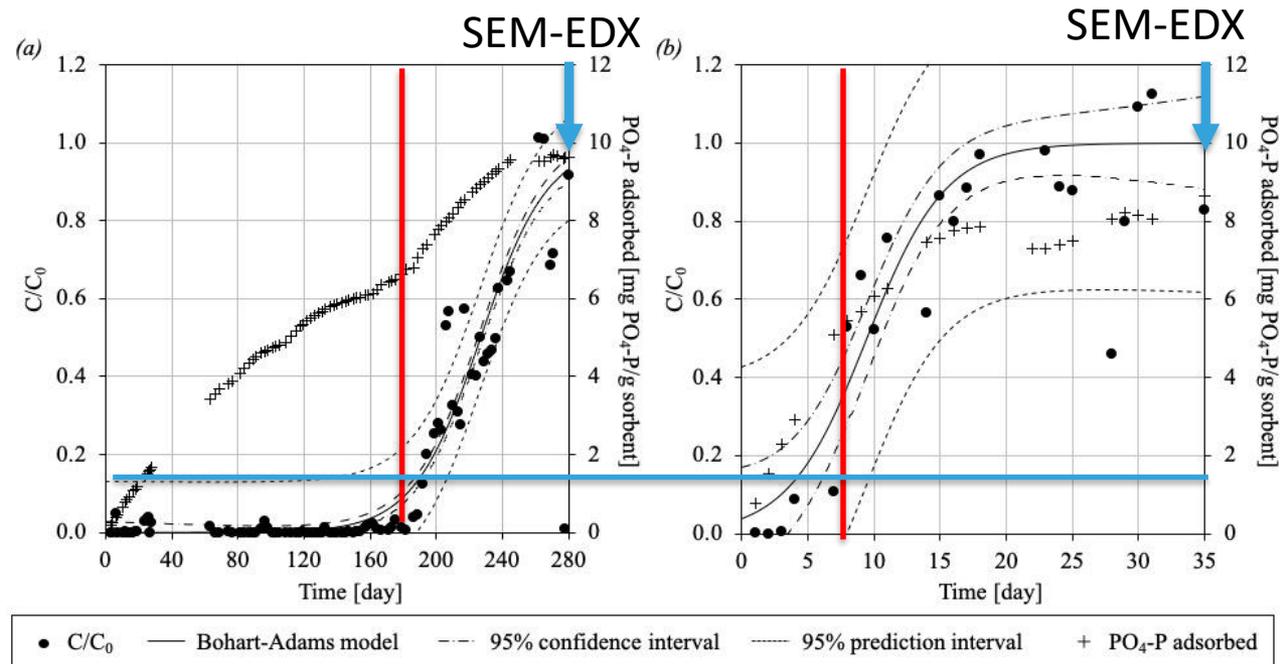


Figure 5: Adsorption column experiments on lab-scale (influent P concentration = 25 mg $\text{PO}_4\text{-P/L}$) with EBCT= 5.5 h (a) and EBCT= 0.5 h (b)

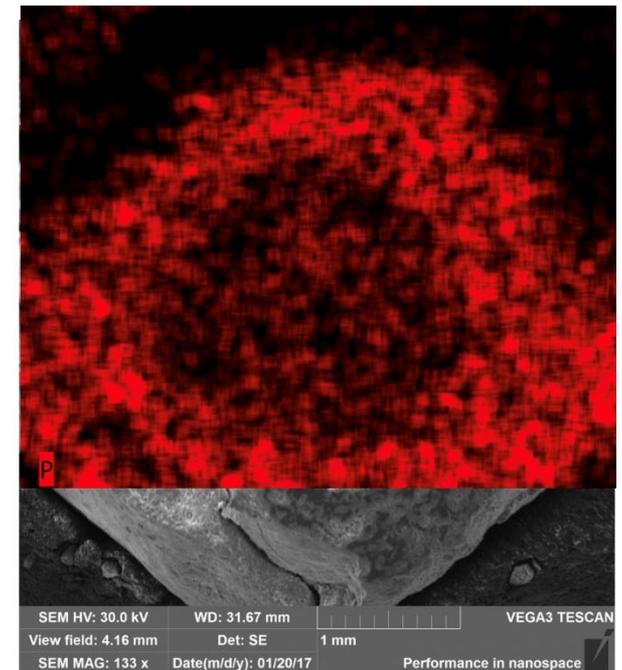
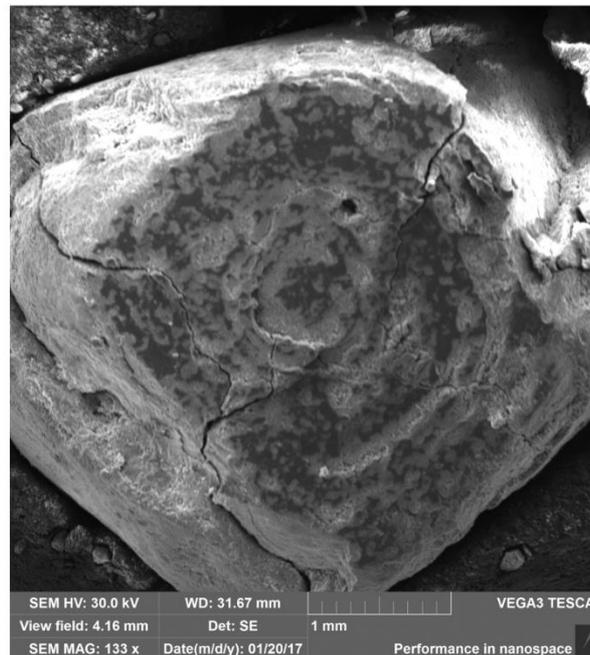
- Figure 5:** The breakthrough curve of column experiments with an Empty Bed Contact Time (EBCT) of **5.5 h** and **0.5 h** results in a breakthrough time of **180 days** and **7 days** respectively.

Results & Discussion

SEM-EDX analysis

- Energy-dispersive X-ray (EDX) Analysis with a Scanning Electron Microscope (SEM) of saturated ICS from two column experiments.
- **Figure 6:** SEM-EDX of saturated ICS of column experiment with **EBCT of 0.5 h**. The phosphate is mainly adsorbed at the outer layers of granules.

polished ICS granules
embedded in a resin

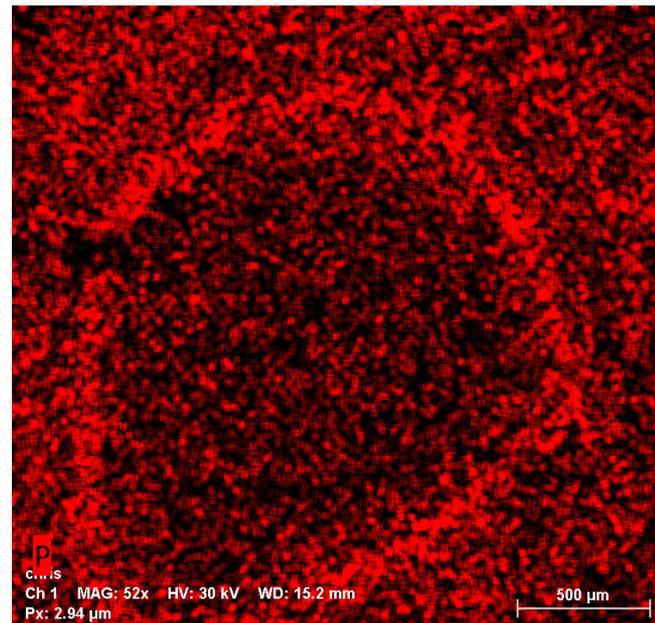


Results & Discussion

SEM-EDX analysis

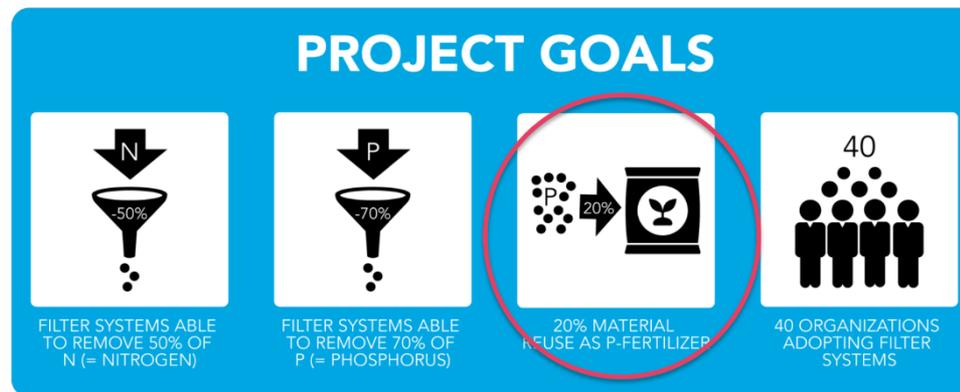
- Energy-dispersive X-ray (EDX) Analysis with a Scanning Electron Microscope (SEM) of saturated ICS from two column experiments.
- **Figure 7:** SEM-EDX of saturated ICS of column experiment with **EBCT of 5.5 h.** phosphorous is accumulated at the sand core of the granule = phosphorous migrates towards the core of the granule.

Si – Fe – P analysis by EDX



Conclusions

- Optimal NaOH concentration = 0.5 M
- Optimal contact time = 24 hours or more
- Optimal S/L ratio = 0.10 - 0.05 g/mL
- P-desorption efficiency = 40% @ 0.5 and 1 M NaOH
- Leaching of Fe during the desorption process is a problem
- Desorption of P from the inner layers of the granule will be a problem



- **What to do next?**
 - Investigating whether other adsorption materials are better suited for desorption: Vito materials and DiaPure?
 - Looking for ways to reduce desorption pH.
 - Carrying out continuous long-term column tests in which cycles of adsorption and desorption are completed → To do in the coming months.



Q & A

Interreg

North Sea Region

NuReDrain

European Regional Development Fund



EUROPEAN UNION

Phosphorus Removal Modelling – From a Single Filter to an Entire Catchment

Stefan Koch, Andreas Bauwe, Bernd Lennartz



INTRODUCTION

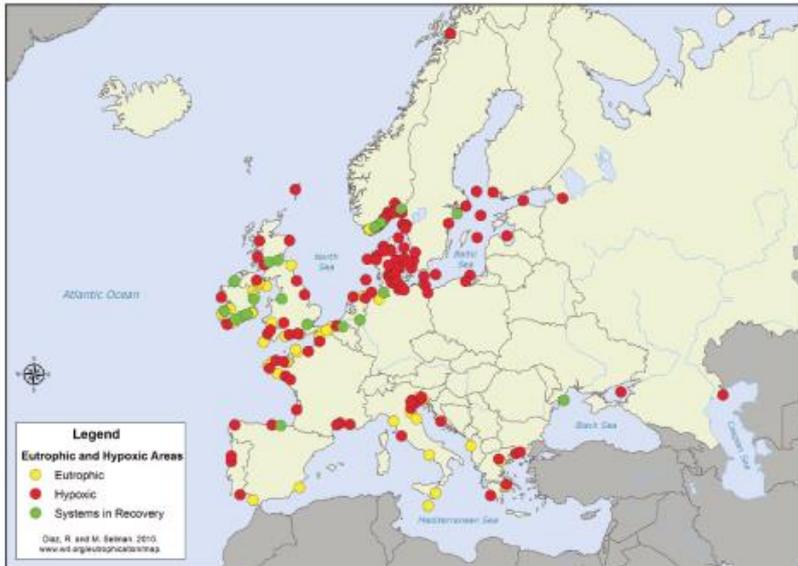
Introduction

- Eutrophication is a major threat to coastal ecosystems
- Harmful algae blooms may cause deoxygenation of water bodies
 - May not only occur in deep waters of oceans
- Nitrogen (N) and phosphorus (P) inputs from agriculture are a critical source of excess nutrients in surface waters

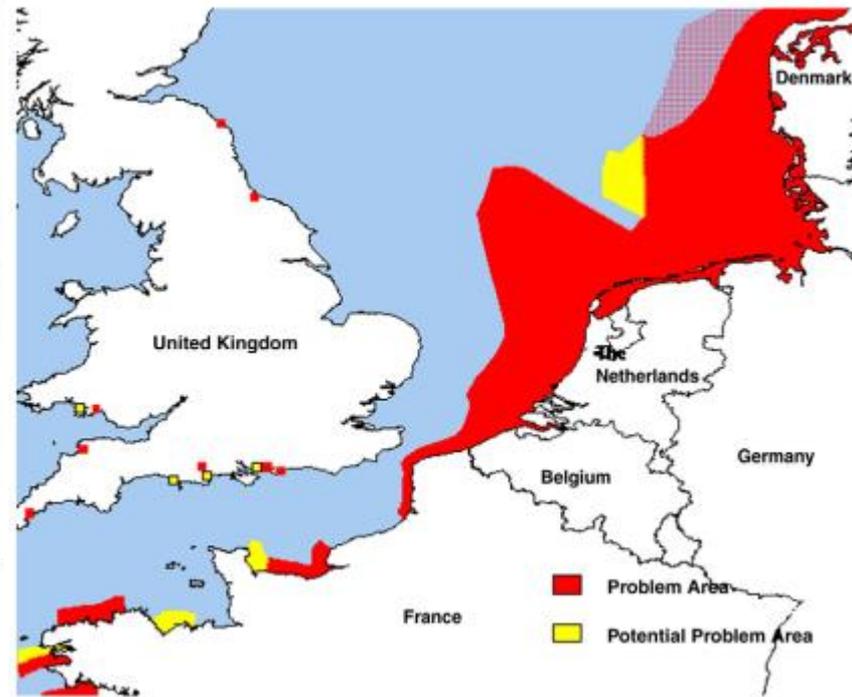


(ESA/ESA/The Guardian/GreatLakesNow)

Eutrophic Areas in the North Sea



IUCN (2019)



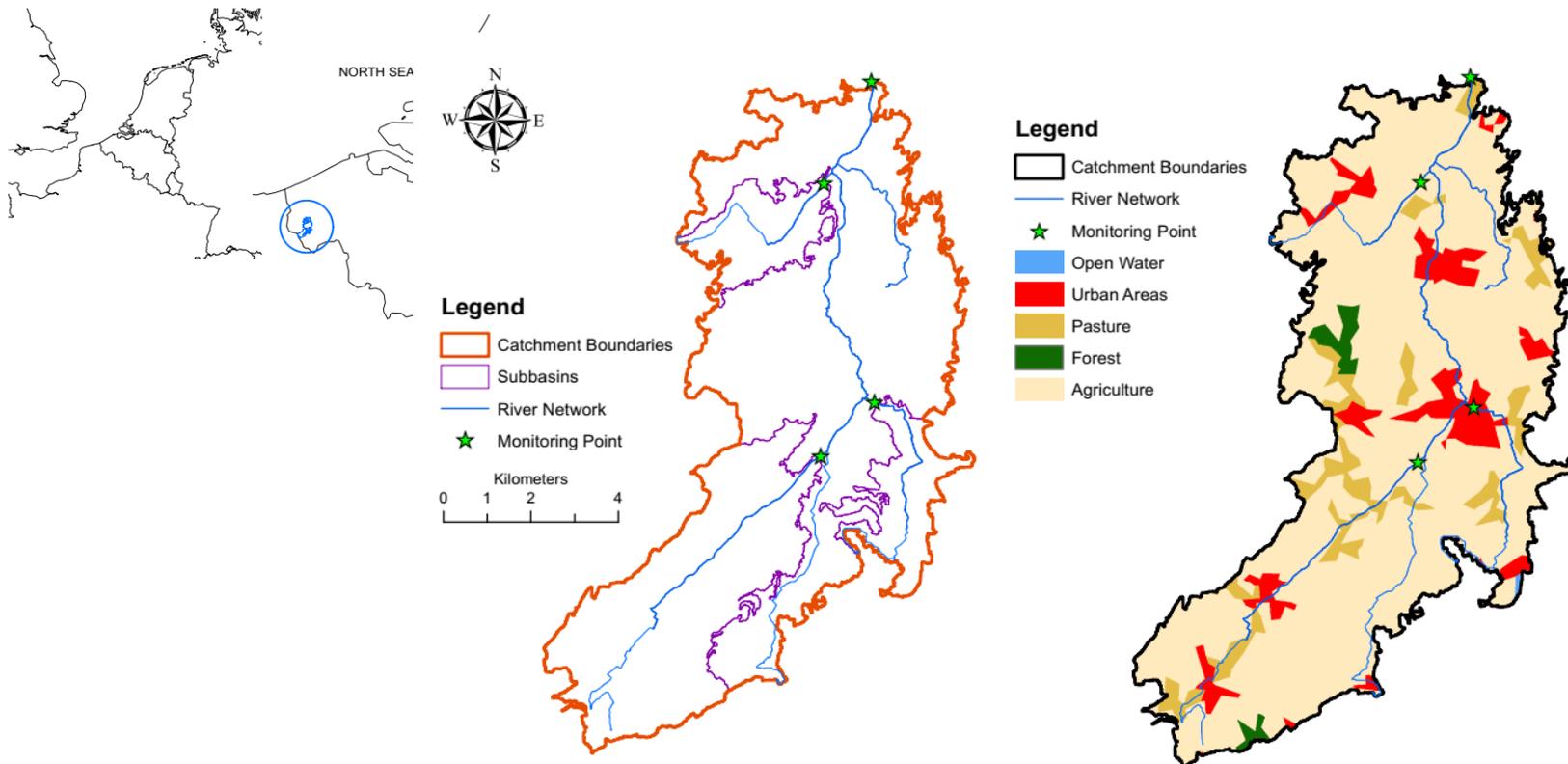
Lenhart et al. (2010)



STUDY SITE AND METHODS

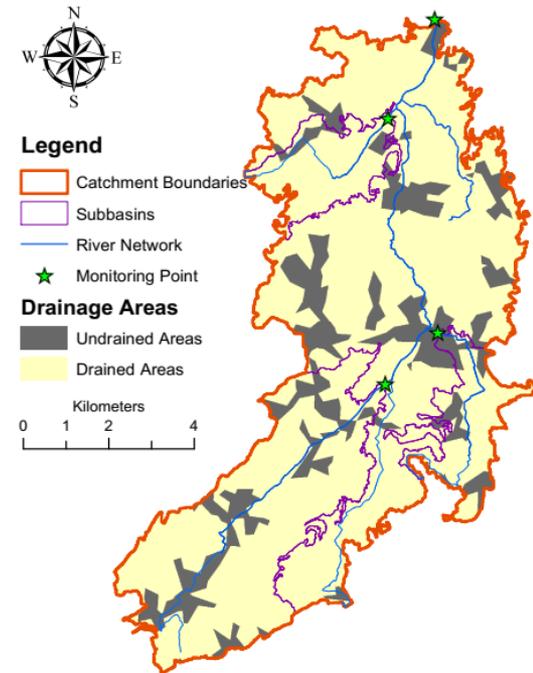
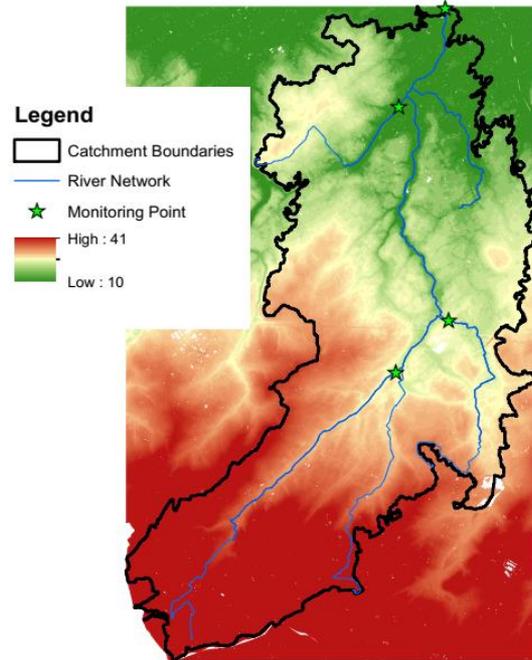
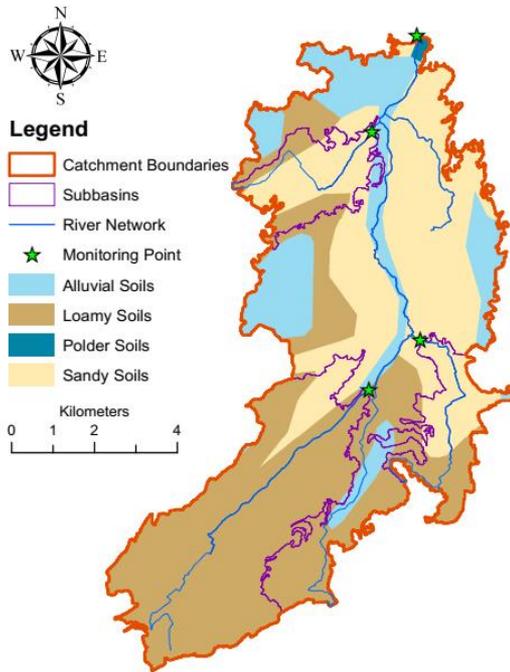
The Kemmelbeek Watershed

- Belgian (Flemish) Watershed, 74 km², situated in Western Belgium
- Agriculture (61.85 km²; 83%) is the major land use in the Kemmelbeek Watershed



The Kemmelbeek Watershed

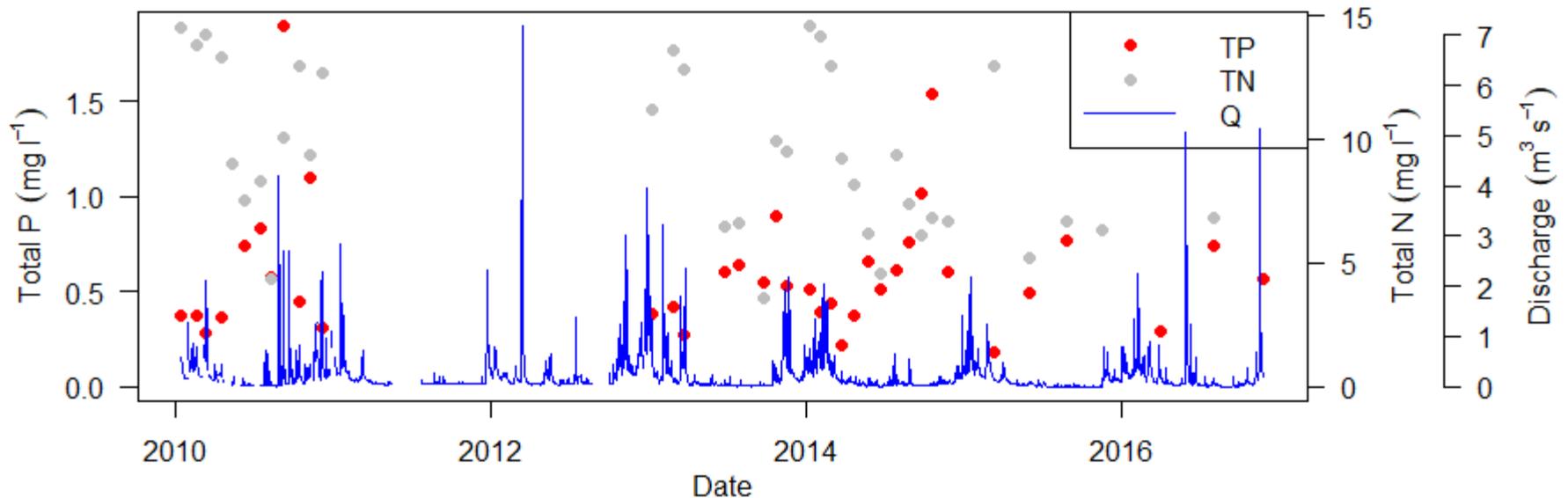
- A heavily tile-drained lowland watershed dominated by loamy soils



The Kemmelbeek Watershed

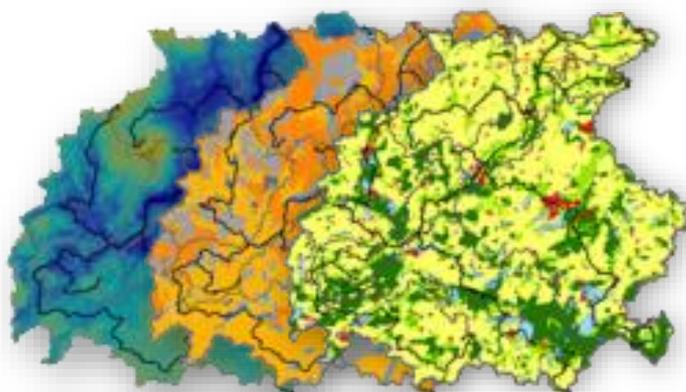
- Elevated TP concentrations in the Kemmelbeek Watershed -> **reduction required**

	mean	max	min	Mean load yr ⁻¹
N (mg/l)	9.5	14.6	3.6	8.9 kg ha ⁻¹
P (mg/l)	0.6	1.9	0.2	0.3 kg ha ⁻¹ (PO ₄)

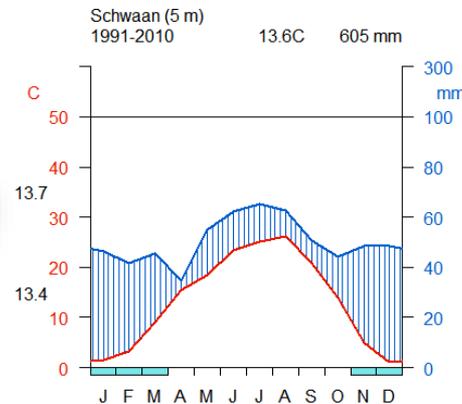


The Soil and Water Assessment Tool (SWAT MODEL)

- **Soil and Water Assessment Tool (SWAT model)** to model streamflow and P loads in tile drains
 - Physically-based eco-hydrological model with a **tile-drainage routine**
 - Spatial resolution: HRU (Hydrological Response Unit)
 - Temporal resolution (according to Input data, hourly to yearly)

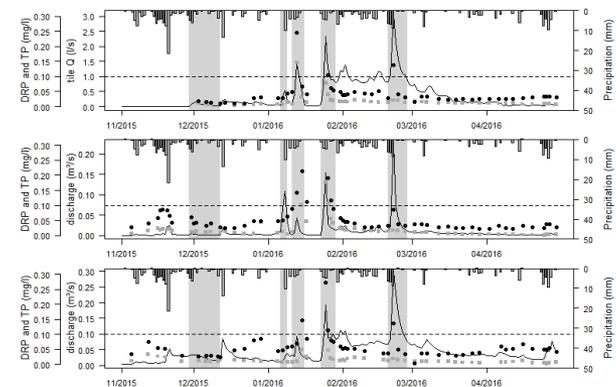


HRU



Weather data

Basic model input

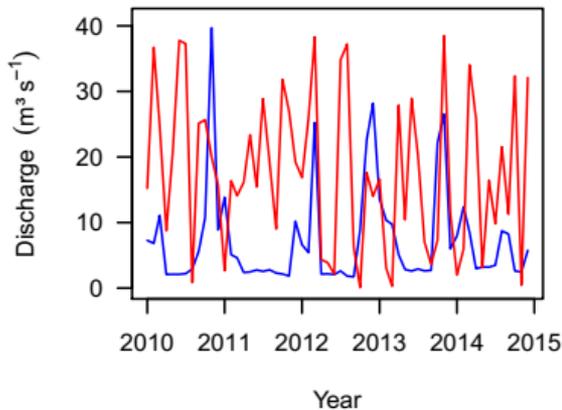


Discharge (+ nutrient, sediment, contaminant data for model calibration)

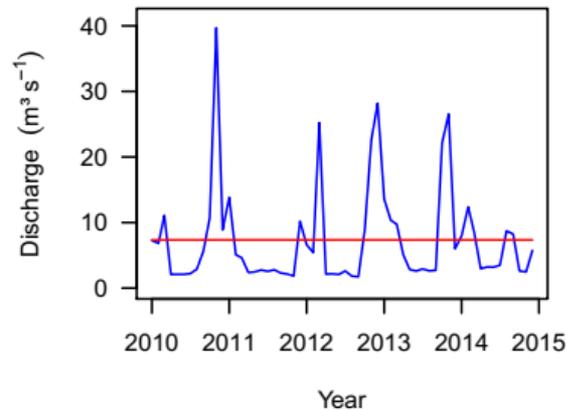
Evaluating Hydrological Models

- **Nash Sutcliffe Efficiency (NSE)** as evaluation index
 - Range from $-\infty$ to 1 (1 is perfect model fit)
 - Values above 0.5 considered as “good”, above 0.75 as “very good”

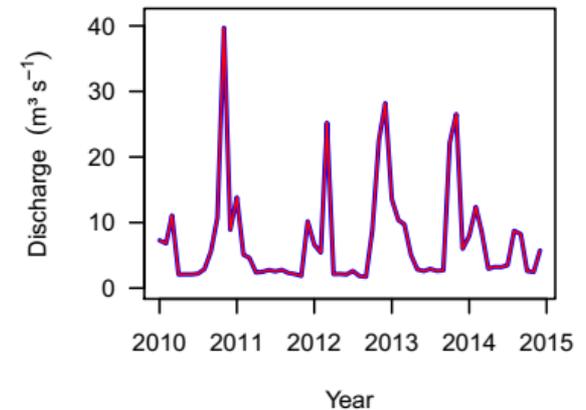
NSE = -3.96



NSE = 0



NSE = 1

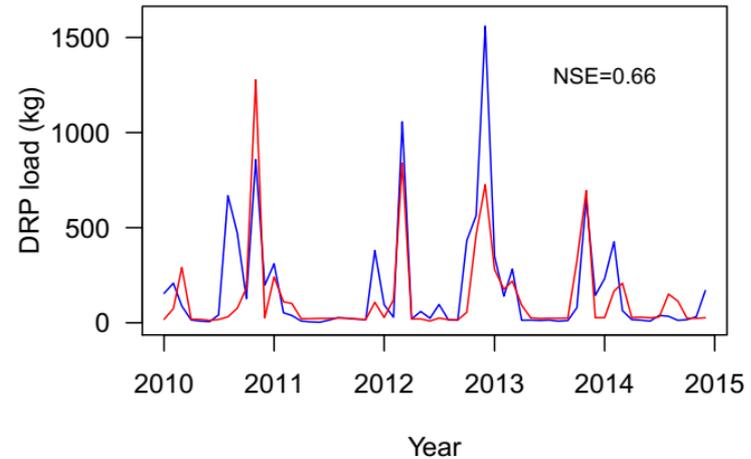
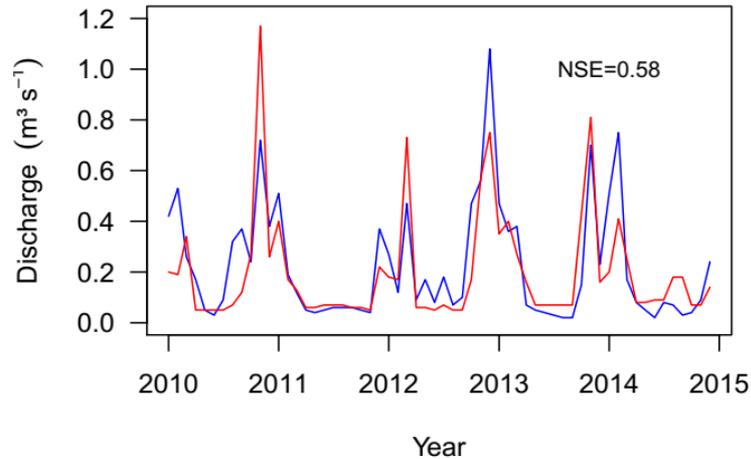




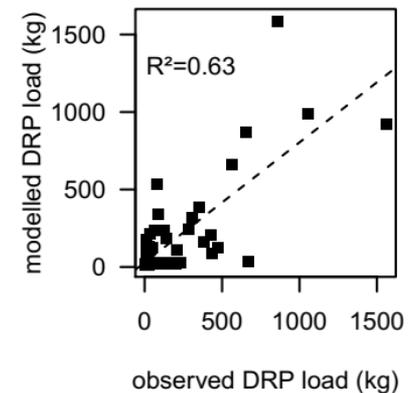
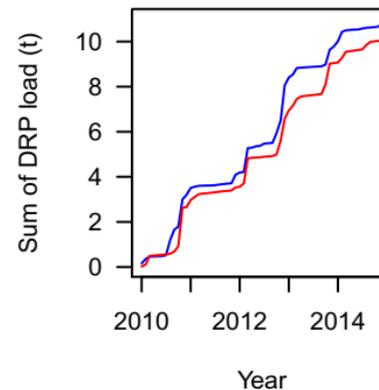
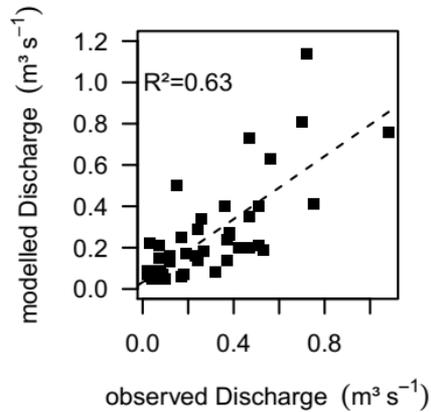
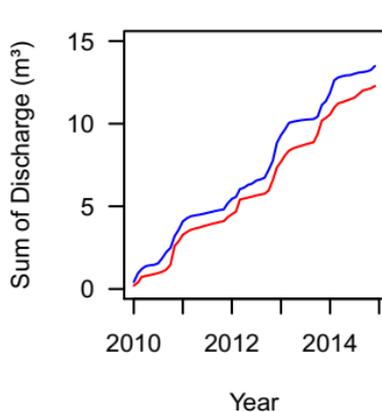
RESULTS

Calibration of Flow and Phosphorus loads

- Measured monthly flow/DRP loads (blue) vs. modelled flow/DRP loads (red) in the calibration period

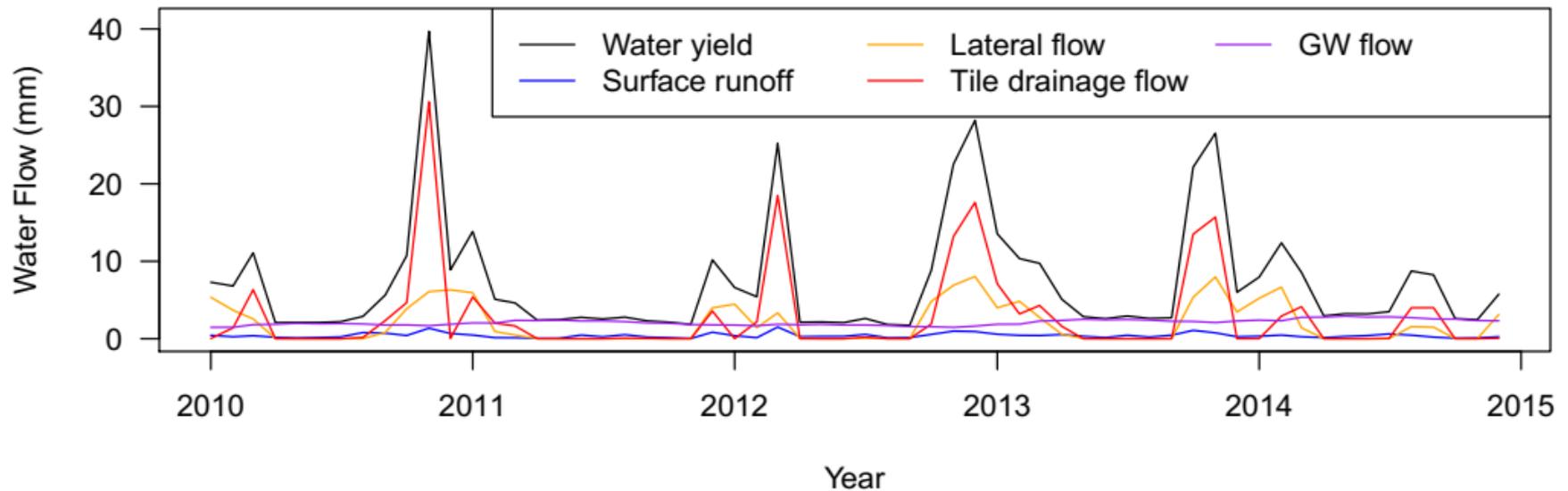


- Sum curves of observed vs. modelled flow and DRP loads and scatterplots of observed and modelled flow and DRP loads in the calibration period

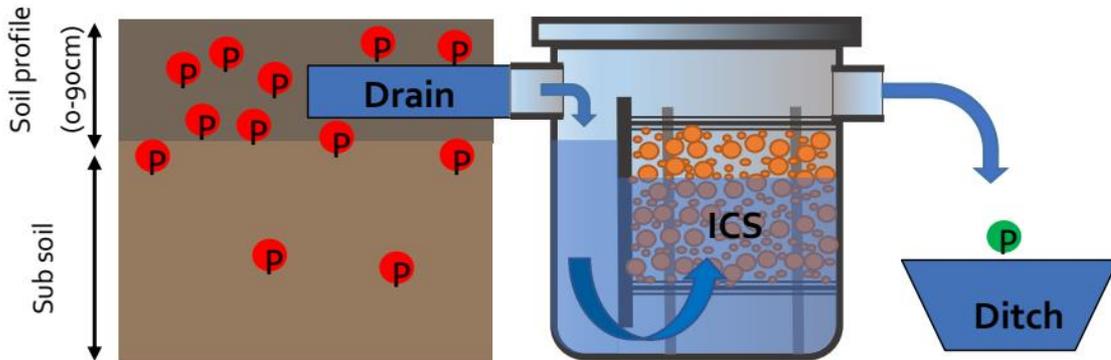


Calibration of Flow and Phosphorus loads

- Realistic **distribution of flow parameters** is crucial for process understanding and the implementation of scenarios



Reduction Scenarios



- **P filters** with iron-coated sand (ICS) in a filter box applied to selected HRUs
- Easy to install
- **High P removal efficiency (80-90%)**
- Low cost installation
- Does not cause any impairment of surface waters



Reduction Scenarios



- P filters applied to different areas of drained agricultural areas

Proportion of area equipped with a filter	Scenarios						
	5	10	15	25	50	75	100
Area (ha)	310	619	929	1548	3095	4643	6191
Number of drainage plots (6 ha per collector drain)	51	103	154	257	515	773	1031
Annual costs (€)	16.218	32.754	48.972	81.726	163.770	245.814	327.858

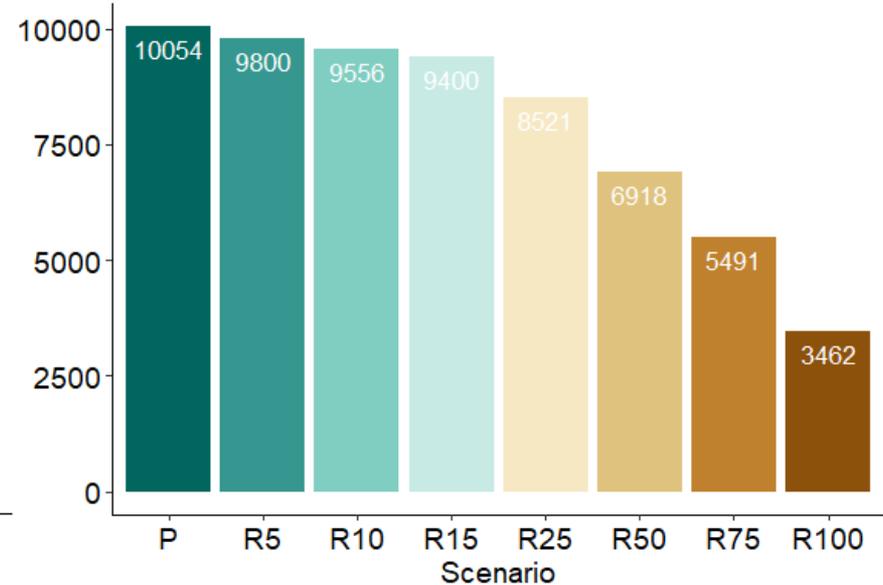
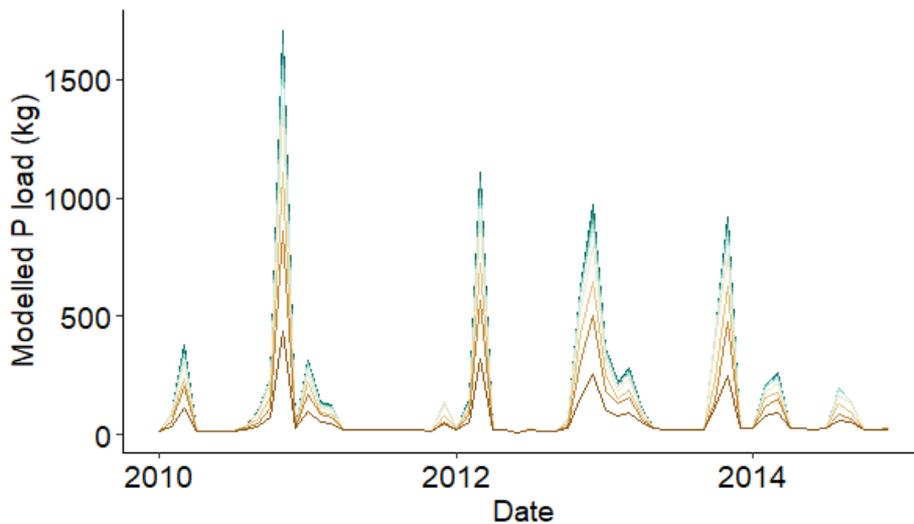
Reduction Scenarios

- P filters applied to different fractions of drained agricultural areas

	Base Model		Reduction Scenarios						
	obs P	mod P	<i>(percentage of agricultural area equipped with P filter)</i>						
			5	10	15	25	50	75	100
P load (kg)	10841	10054	9800	9556	9400	8521	6918	5491	3462
P load reduction (kg)			254	498	654	1533	3136	4563	6592
Reduction (%)			3	5	7	15	31	45	66

Reduction Scenarios

- The installation of P filter may cause a 66% reduction of the total DRP load



- Long-term studies on in-situ filter techniques will improve the development and implementation of scenarios to hydrological models
- In-situ tests of different filter materials will help getting a wide range of scenarios of P reduction
- Using the same approach for developing N reduction scenarios



Thank you for your attention

Q & A

Next seminars

- Friday 2/10 – 10h – 11h30:

Filter technologies for N removal from agricultural waters

<https://northsearegion.eu/nuredrain/>

Acknowledgements

